

Ab initio based microkinetic modelling as a tool to understand and improve controlled polymerization processes

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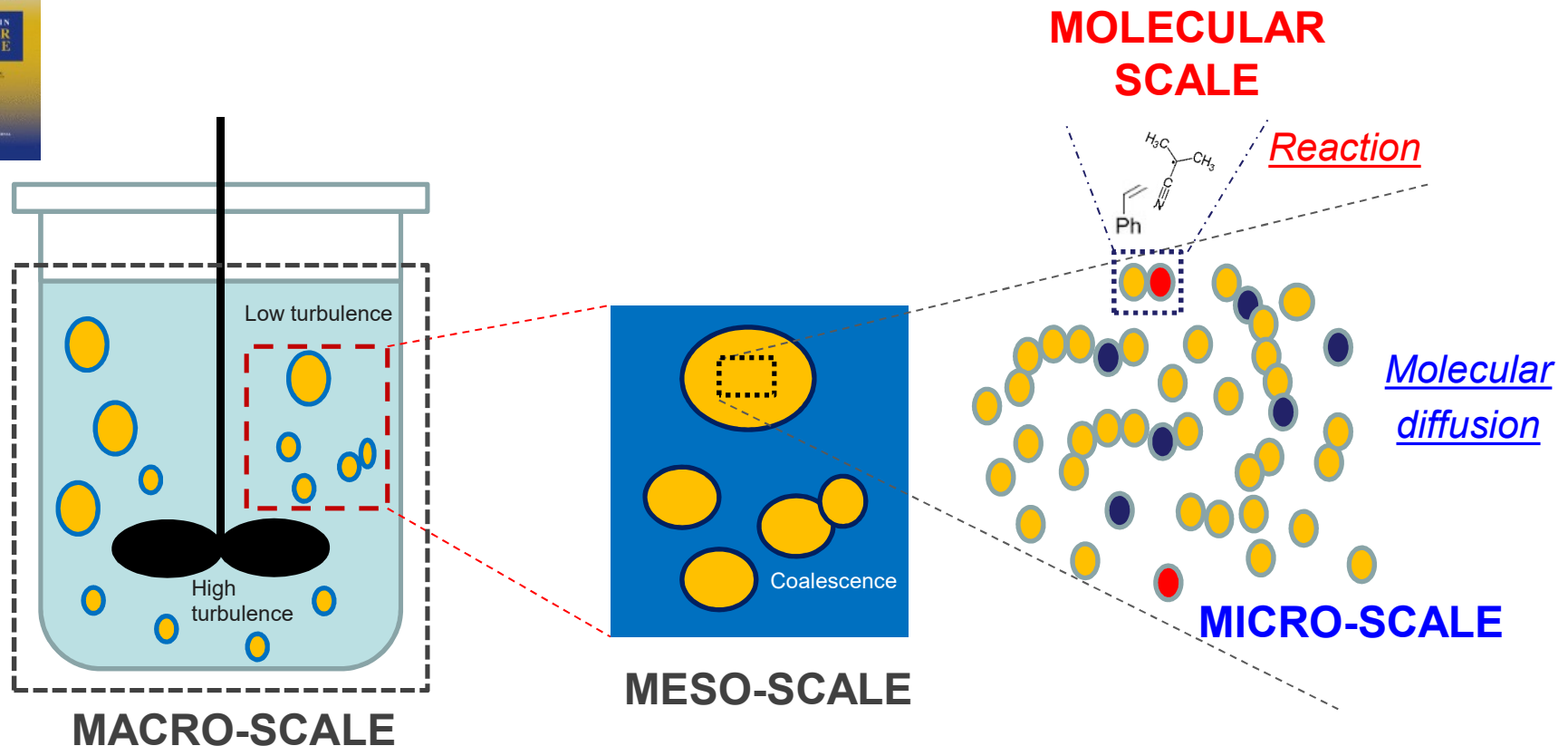
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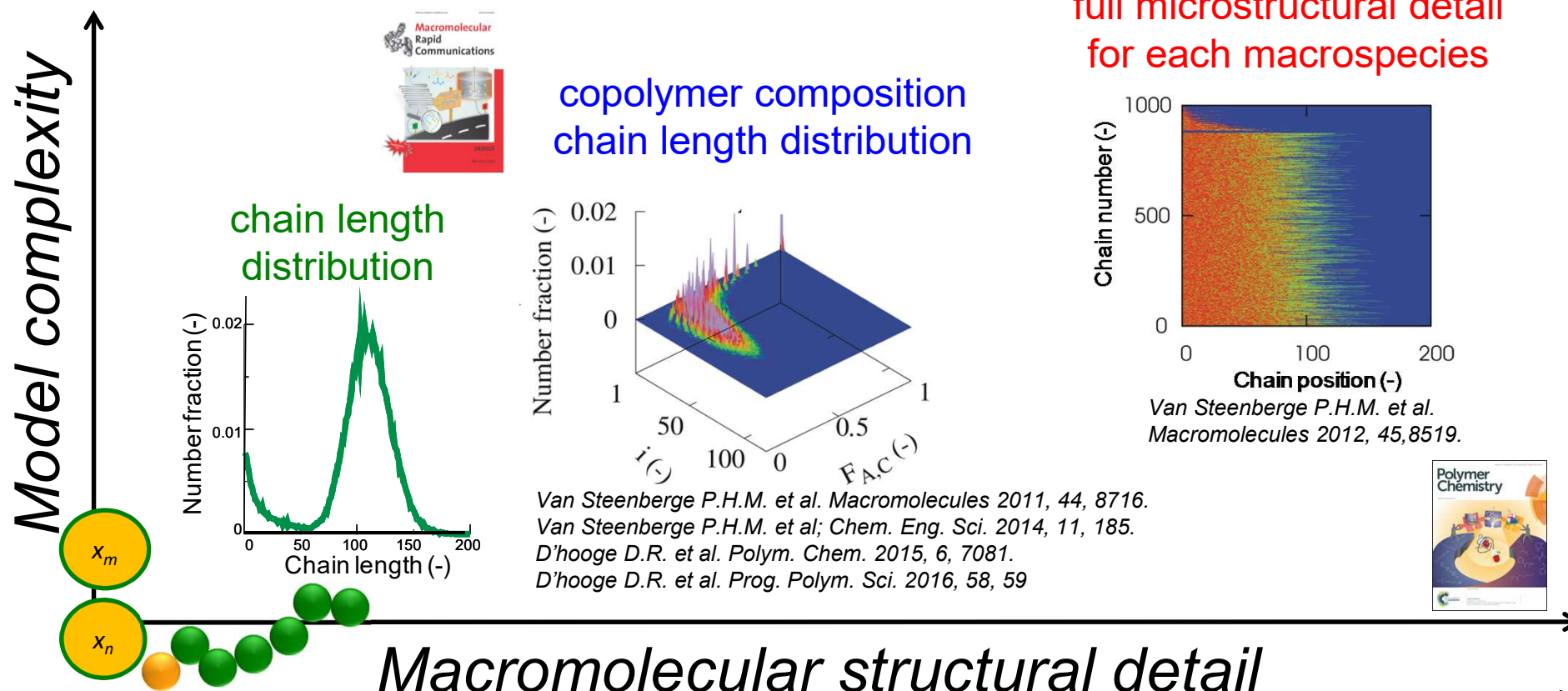
Overview

- Introduction: ab initio based multi-scale modelling
- Proof of principle: RAFT polymerization of styrene
 - computational method: model assumptions
 - validation of computational method
- Design of sequence controlled copolymers
- Insight in monomer sequence formation in gradient copolymers
- Conclusions

Multi-scale modelling: polymerization processes



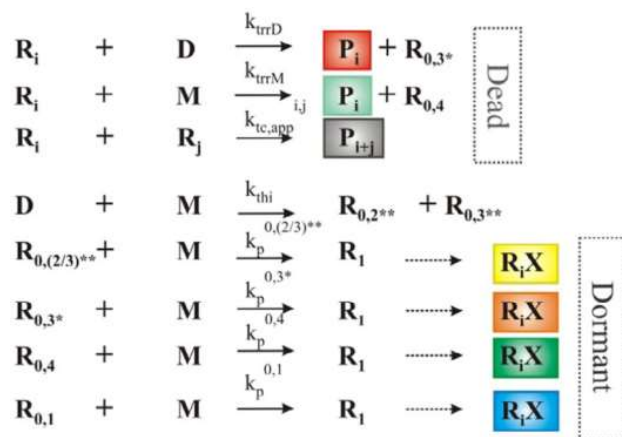
Generic modelling toolkit



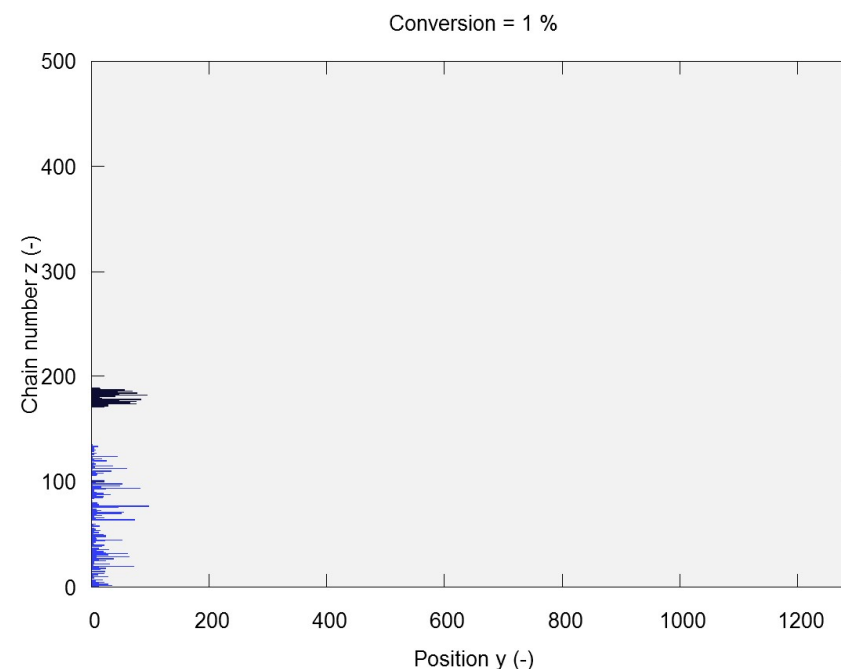
Matrix-based kinetic Monte Carlo algorithm

Blockbuilder-MA mediated polymerization of styrene (including all side reactions)

- tracking all reaction events leading to formation of each macromolecule (10^5 macromolecules)
- visualization: differentiation of macromolecules according to initiation/termination mechanism



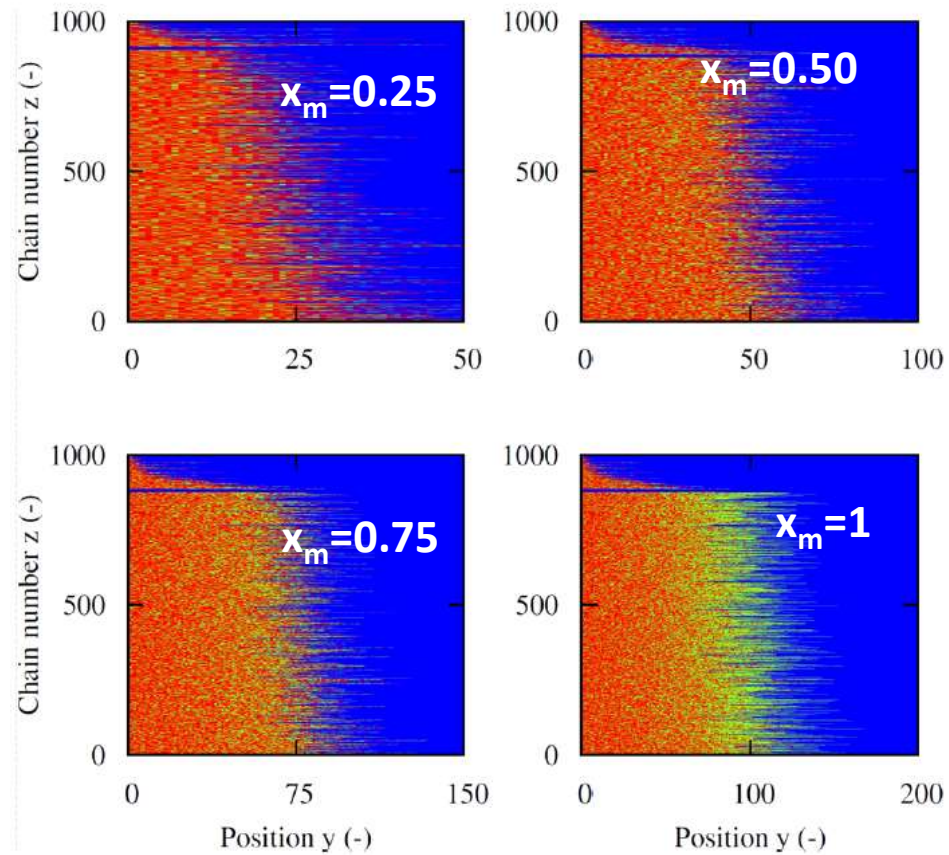
- data analysis: loss of control (∇ and ∇) mainly due to thermal initiation and chain transfer to dimer



$T = 120^\circ\text{C}$; $\text{TCL} = 1000$

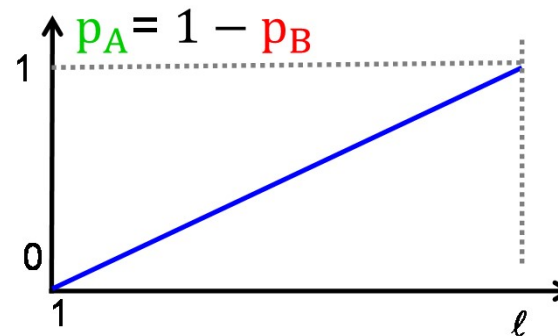
Linear gradient copolymers





linear gradient copol
n-BuA/MMA via ATRP



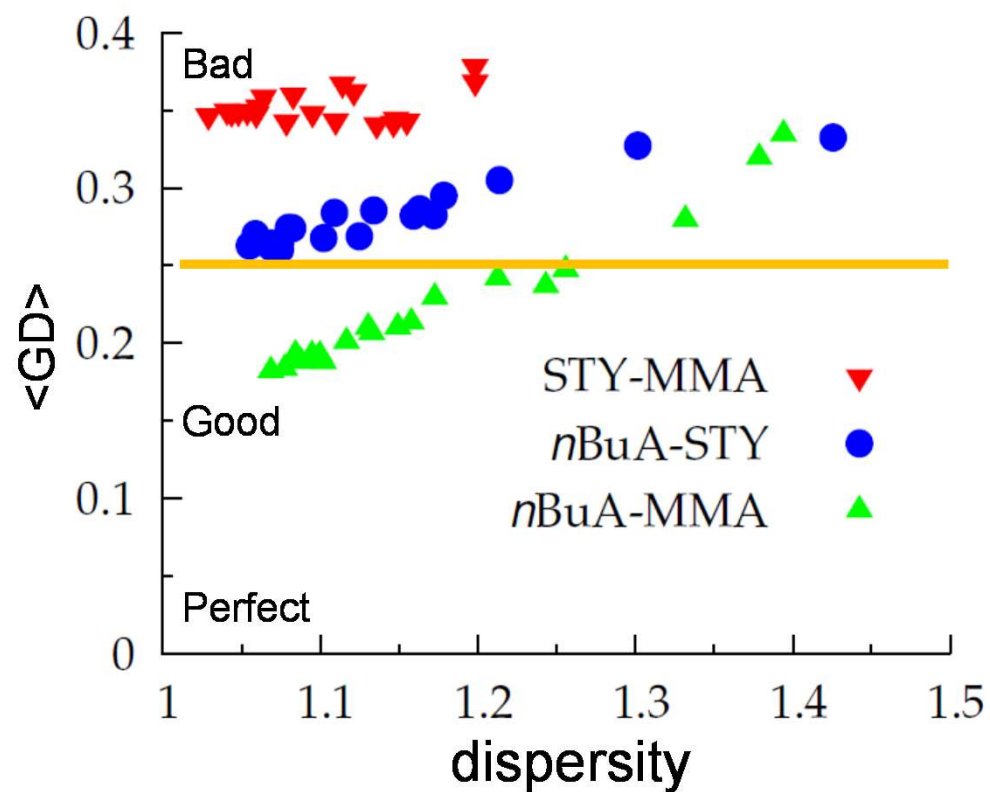
Classification of gradient quality via $\langle \text{GD} \rangle$ value

- Mathematical definition of **perfect linear gradient chain**



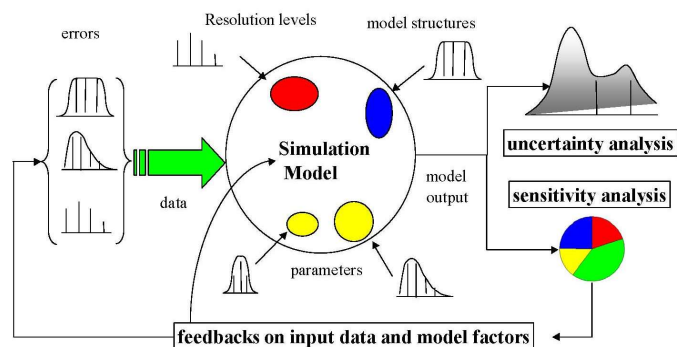
| | | |
|-----------|--|---|
| "perfect" |  | $\langle \text{GD} \rangle \leq 0.06$ |
| good |  | $0.06 \leq \langle \text{GD} \rangle \leq 0.25$ |
| bad |  | $0.25 \leq \langle \text{GD} \rangle < 1.0$ |
| very bad |  | $\langle \text{GD} \rangle = 1.0$ |

<GD> correlates with dispersity

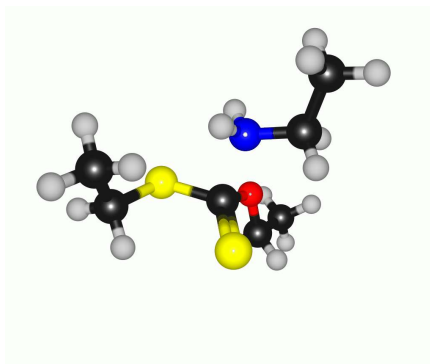
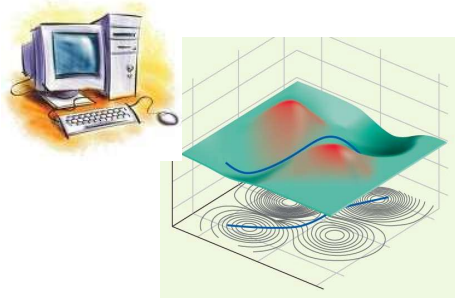


Kinetics elementary reactions

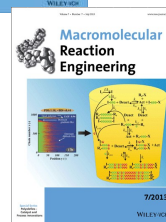
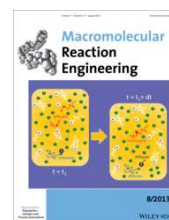
•experiment



•quantum chemistry

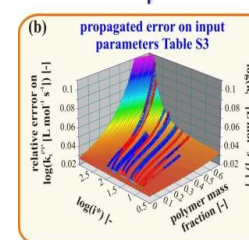
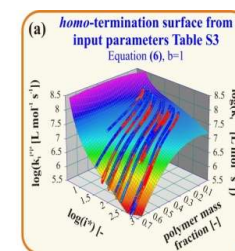


Including molecular diffusion



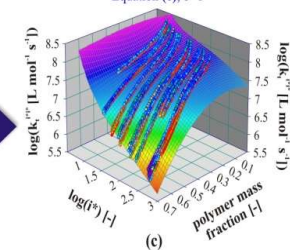
$$\frac{1}{k_{a,app}} = \frac{1}{k_{a,chem}} + \frac{1}{K_{eq}k_{da,diff}}$$

$$\frac{1}{k_{da,app}} = \frac{1}{k_{da,diff}} + \frac{1}{k_{da,chem}}$$

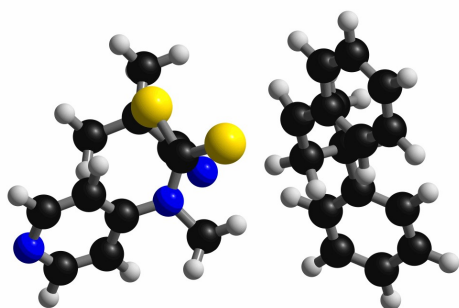


RAFT-CLD-T

improved *homo*-termination surface
Equation (6), b=1

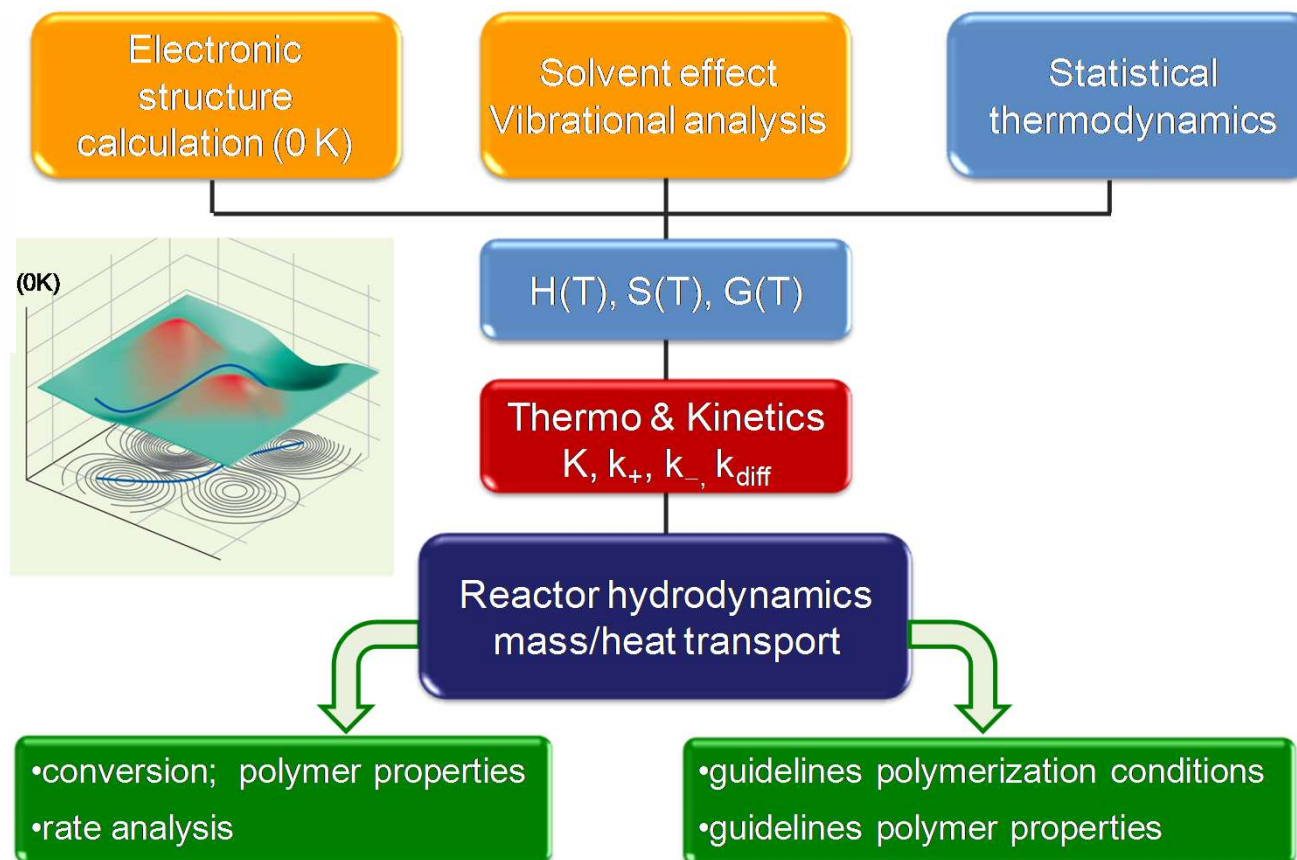


Ab initio based multi-scale modelling: approach

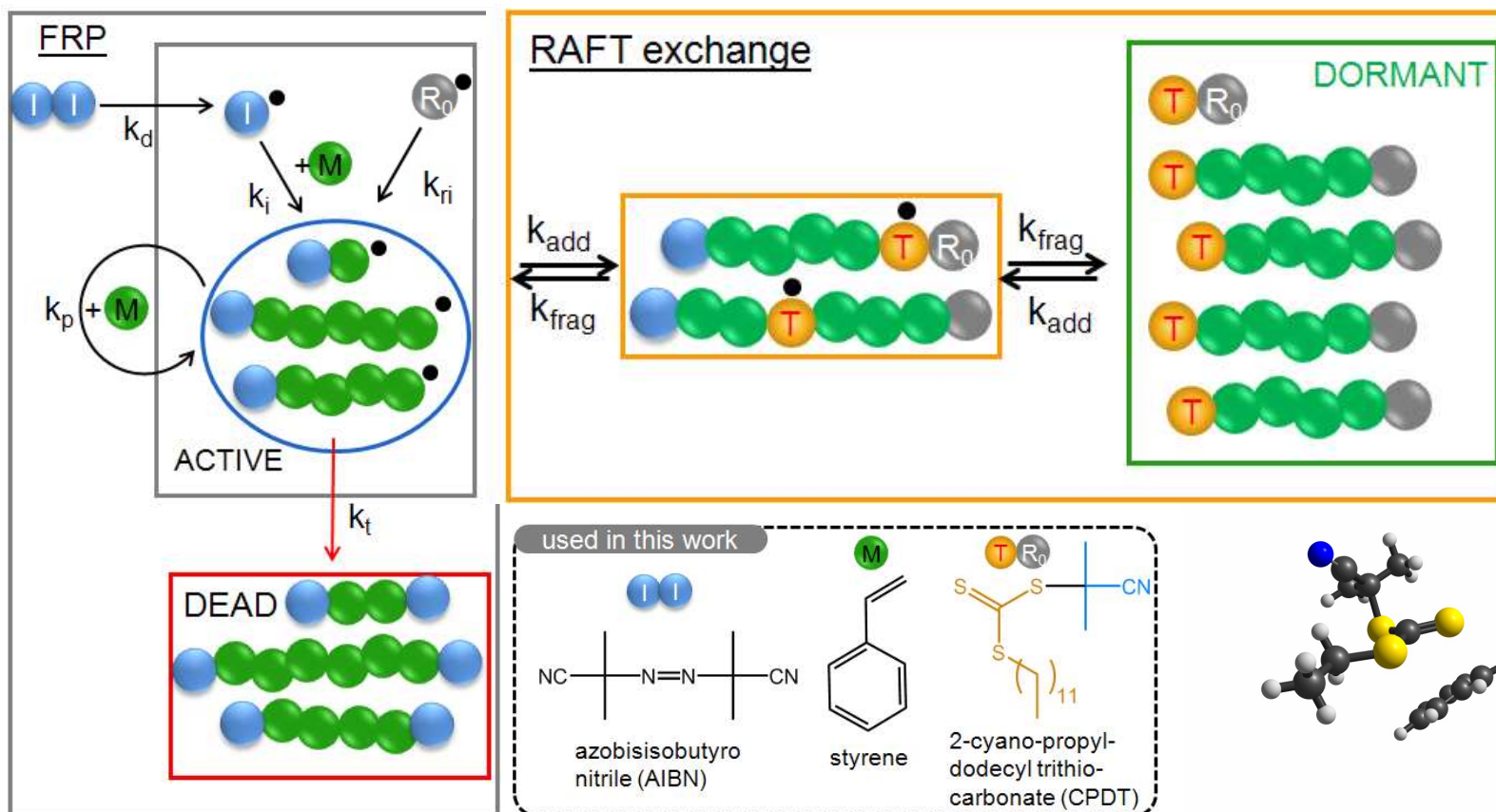


trade off between:

- accuracy
- computational cost



Proof of principle: RAFT of styrene



Computational method

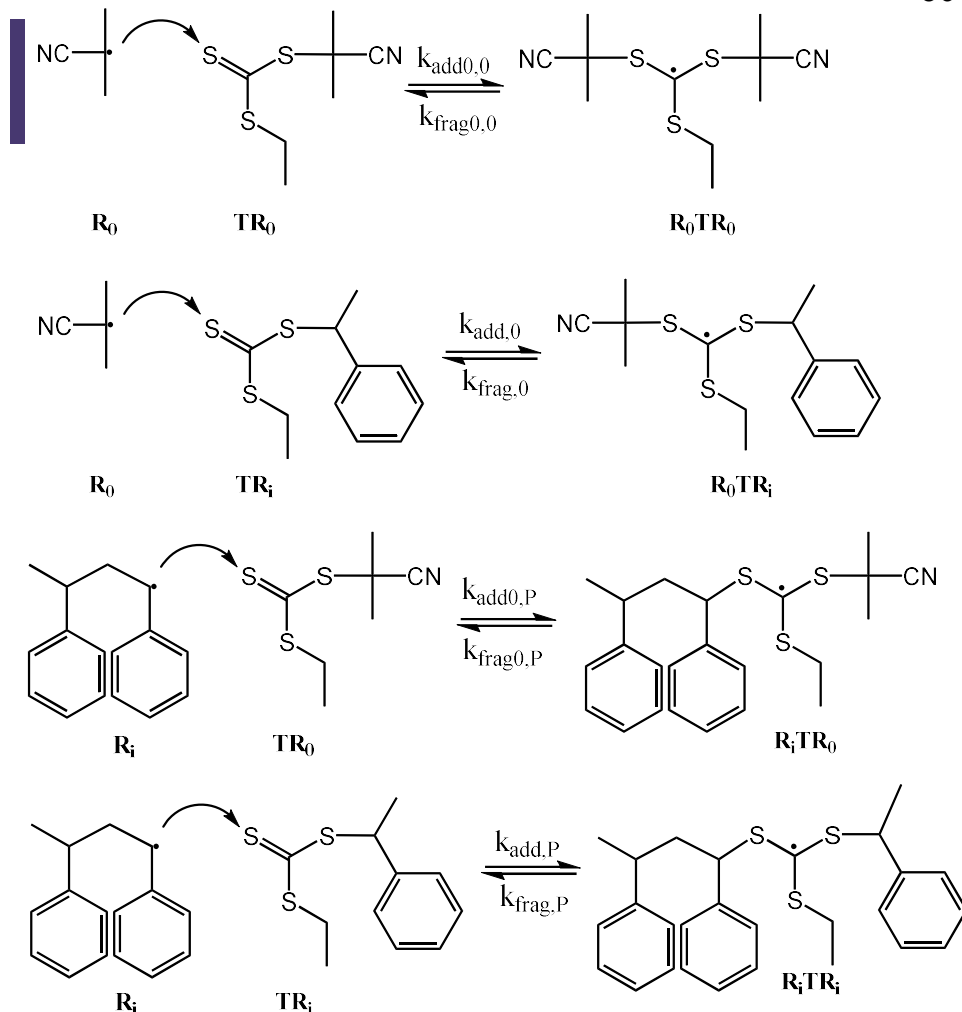
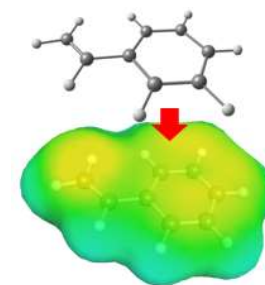
Model assumptions

- dimer radical to model macroradical^a
- ethyl group to model dodecyl group

Ab initio calculation

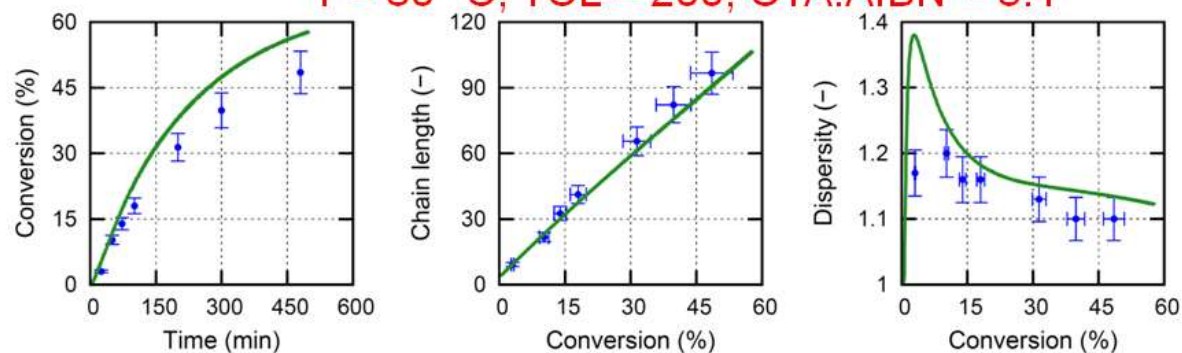
- scan conformers: B3LYP/6-31G(d)
- geometry optimization and frequencies: B3LYP/6-31G(d)
- 'single point' electronic energy: M06-2X/6-311+G(d,p)

Solvation via COSMO-RS



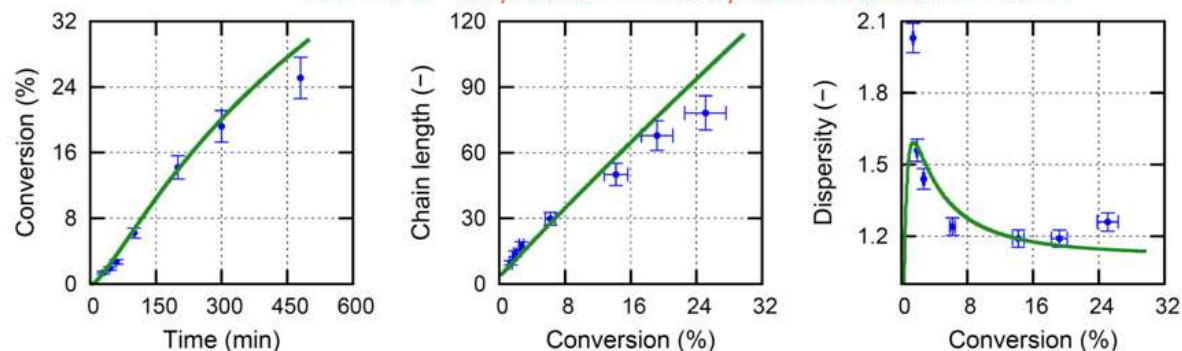
Ab initio based microkinetic modelling

$T = 80\text{ }^{\circ}\text{C}$, $\text{TCL} = 200$, $\text{CTA:AIBN} = 5:1$



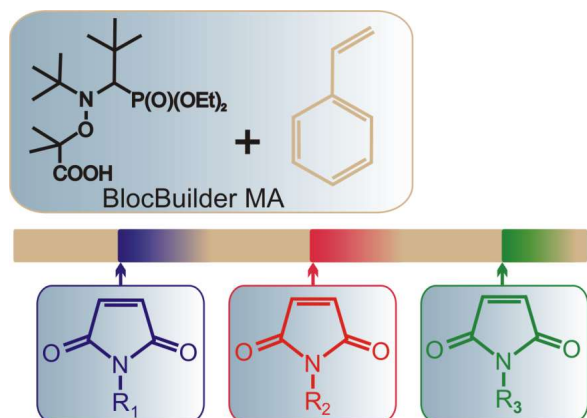
- very good agreement with experimental data in broad range of conditions

$T = 70\text{ }^{\circ}\text{C}$, $\text{TCL} = 400$, $\text{CTA:AIBN} = 5:1$



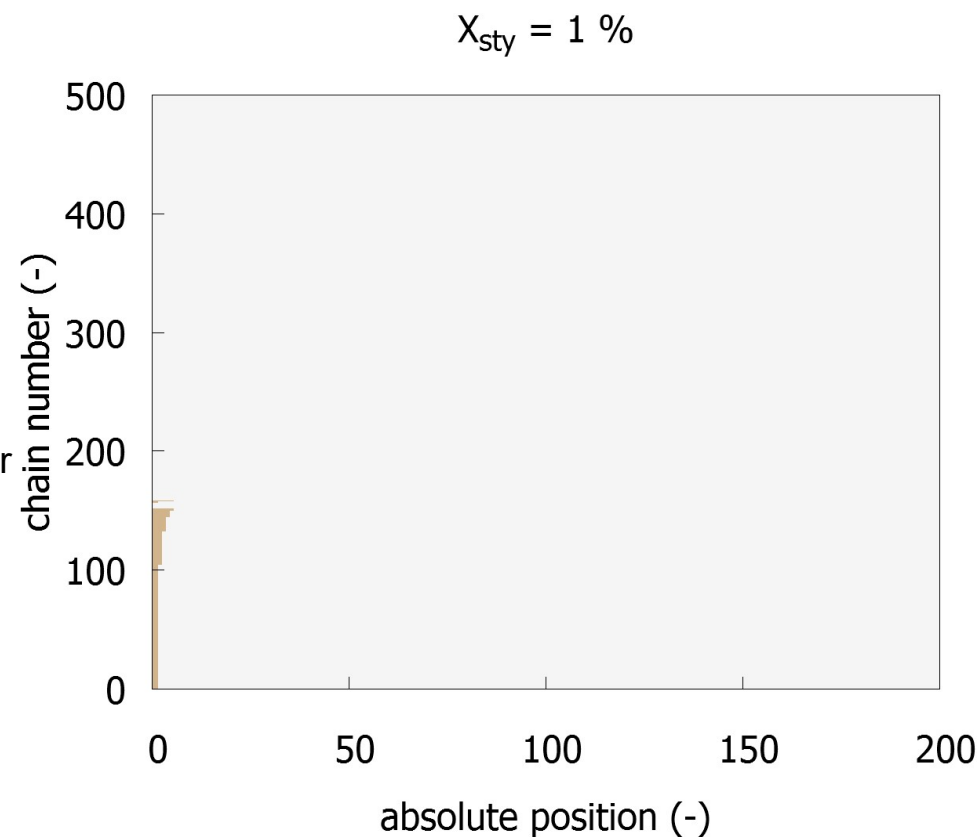
- computational approach validated

Model-based design: sequence controlled polymers



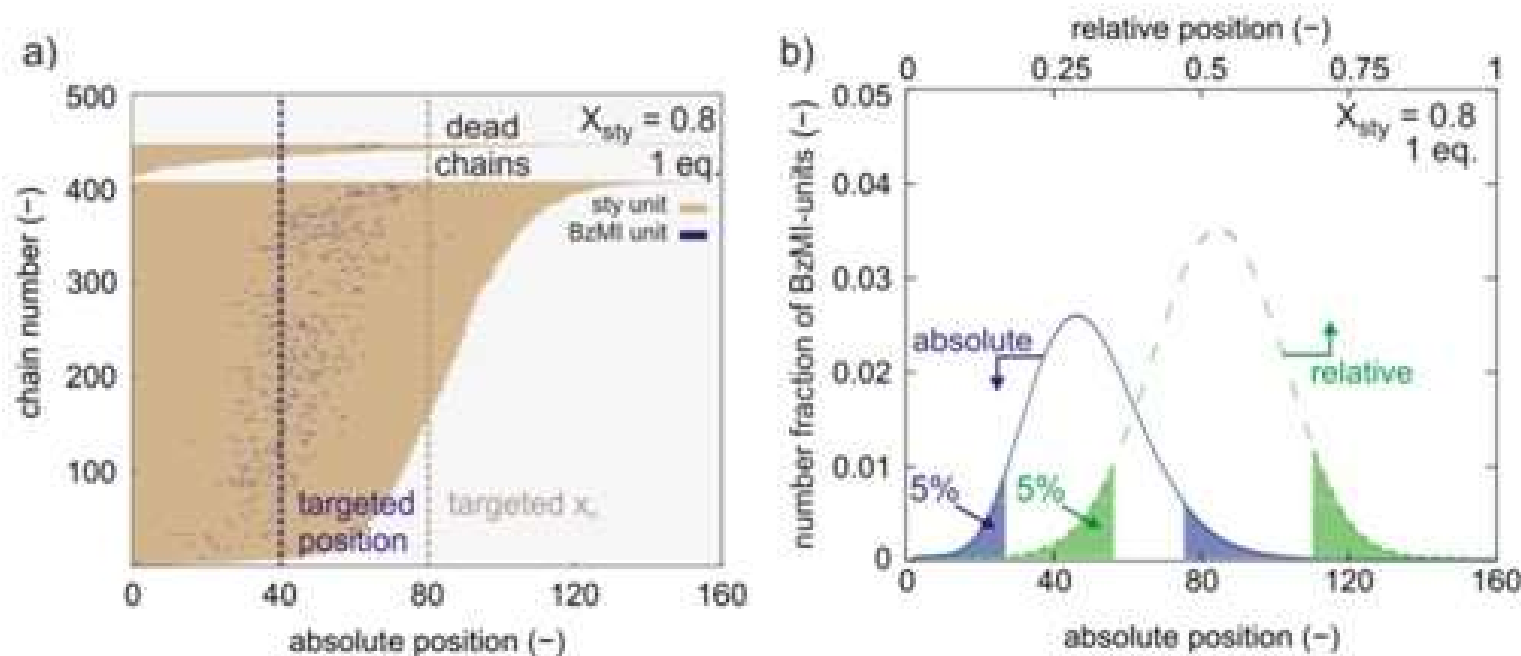
- Electron-donor (e.g. styrene) and electron-acceptor (e.g. N-substituted maleimide) comonomers
high cross-propagation
allows 'local' functionalization using CRP techniques
- CRP techniques are statistical processes:
uncertainty of functional monomer placement

In collaboration with Dr. J.-F. Lutz



Design of monomer addition program (1)

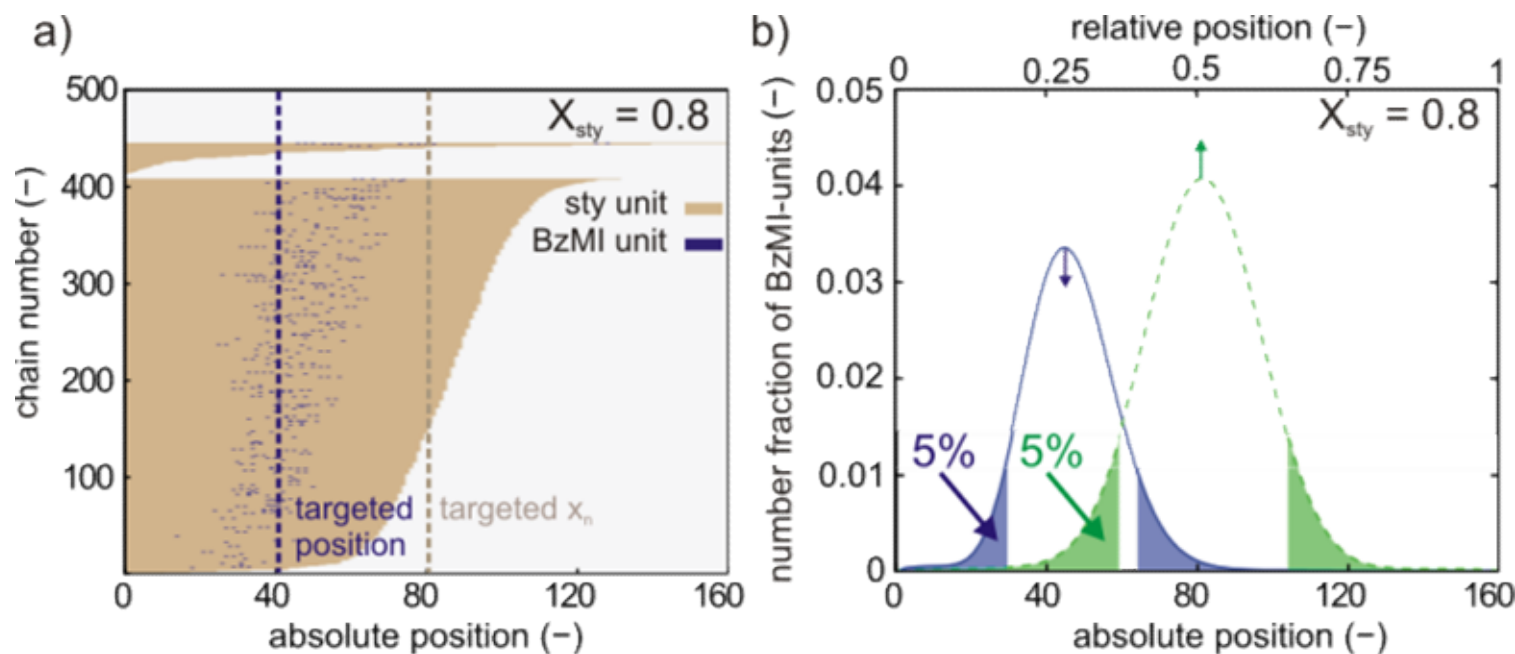
$T = 120^{\circ}\text{C}$; $[\text{Sty}]_0 : [\text{R}_0\text{X}]_0 : [\text{BzMI}]_{\text{addition point}} = 100:1:1\text{eq}$



1 eq BzMI injected at $X_{\text{sty}} = 0.4$

Design of monomer addition program (2)

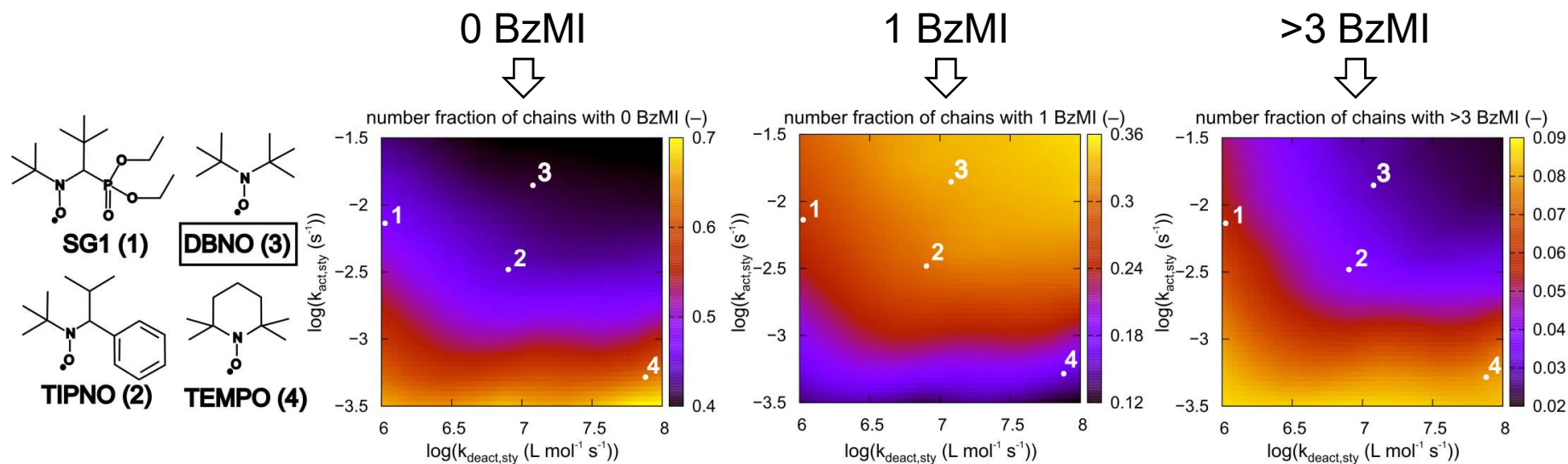
$T = 120^{\circ}\text{C}$; $[\text{Sty}]_0 : [\text{R}_0\text{X}]_0 : [\text{BzMI}]_{\text{addition point}} = 100:1:1\text{eq}$



half of total styrene amount is added initially; at $X_{\text{sty}} = 0.80$ all of the BzMI is added; at $X_{\text{sty}} = 0.90$ remaining amount of styrene is added

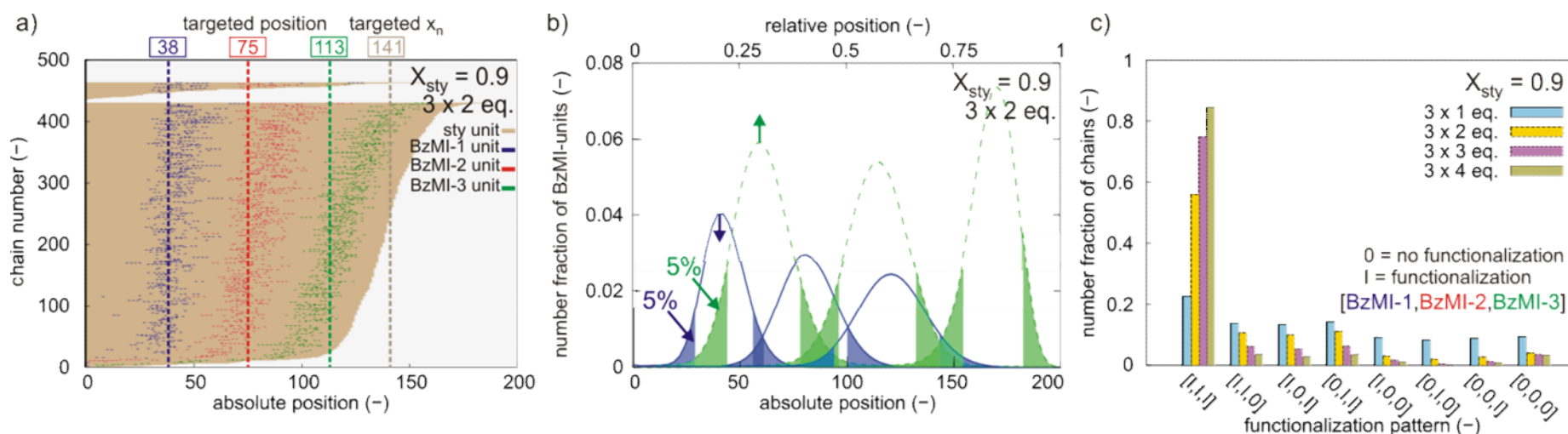
Selection of nitroxide

$T = 120^{\circ}\text{C}$; $[\text{sty}]_0/[\text{BzMI}]_{\text{AP}}/[\text{X}]_0/[\text{BPO}]_0 = 100/1/1/0.71$



Improved BzMI-unit distribution along chains with DBNO

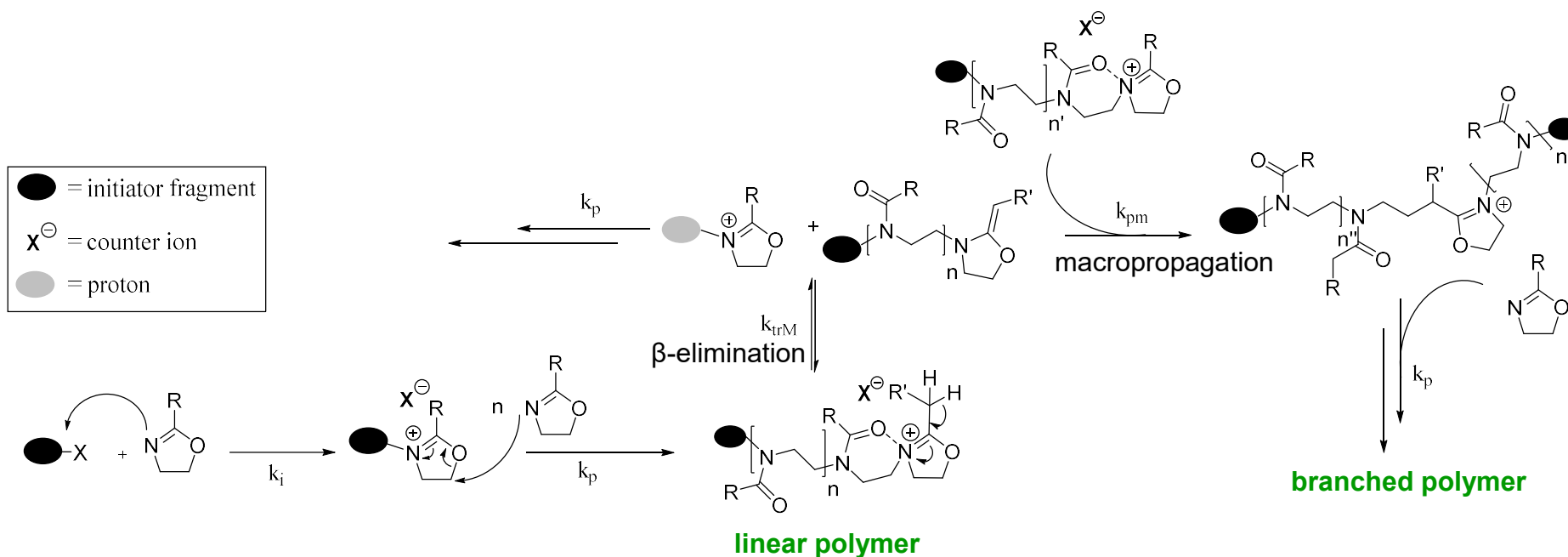
Design of sequence controlled copolymer synthesis



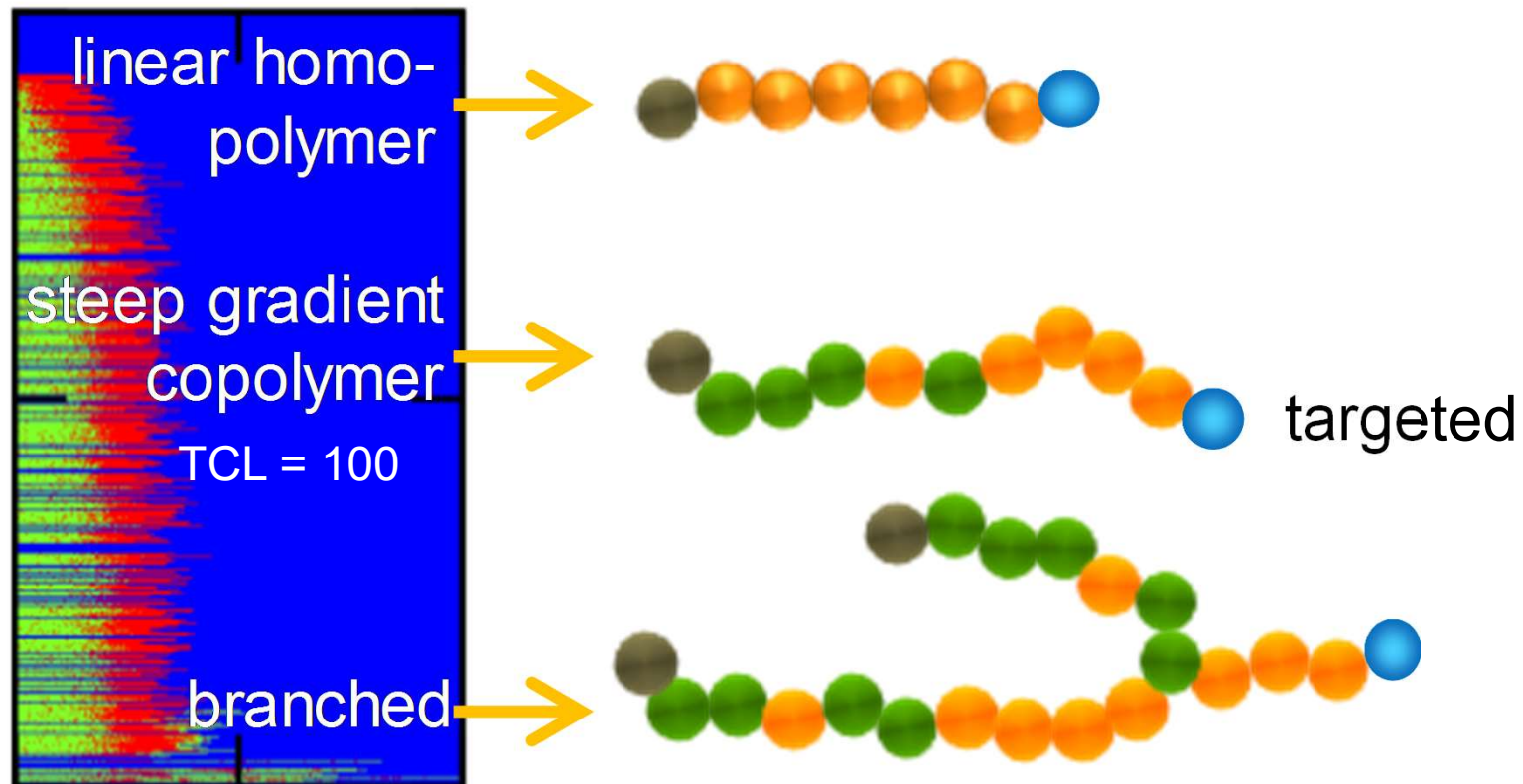
NMP styrene with 3 BzMI additions ; 120°C; $[Sty]_0 : [R_0X] : [BzMI-1]_{AP1} : [Sty]_{AP2} : [BzMI-2]_{AP3} : [Sty]_{AP4} : [BzMI-3]_{AP5} : [Sty]_{AP6} = 47:1:eq.:45:eq.:45:eq.:13; eq. each time defined with respect to R_0X ; addition point (AP) 1,3 and 5 at $X_{sty} = 0.8$ and addition point 2, 4 and 6 at $X_{sty} = 0.9$$

Gradient copoly(2-oxazolines) via CROcoP

Cationic Ring-Opening coPolymerization (CROcoP) of MeOx and PhOx initiated by MeOTs in acetonitrile



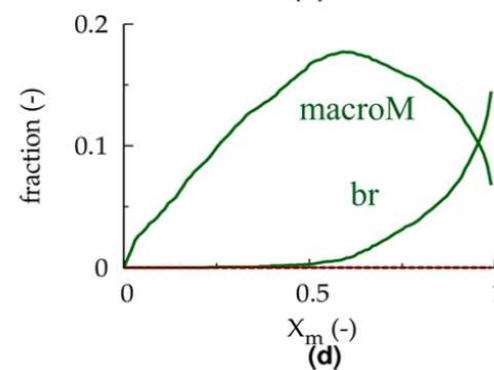
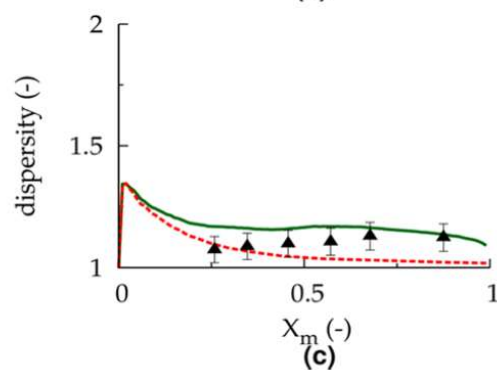
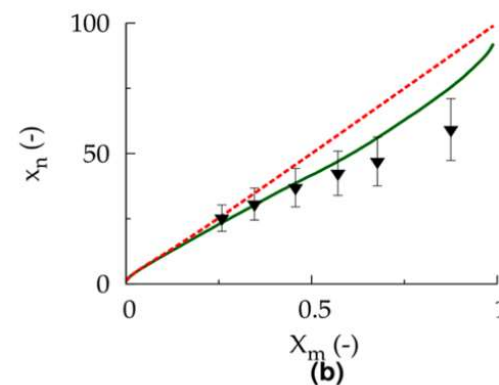
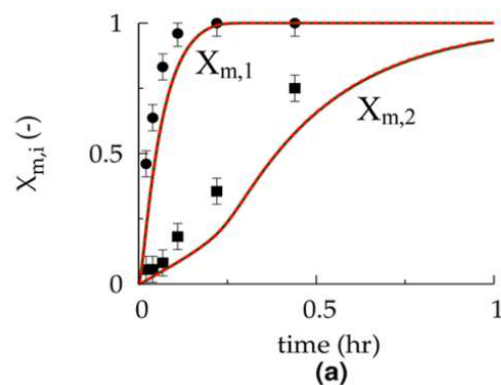
Target: steep MeOx-PhOx gradient



Effect of chain transfer in CROcoP (1)

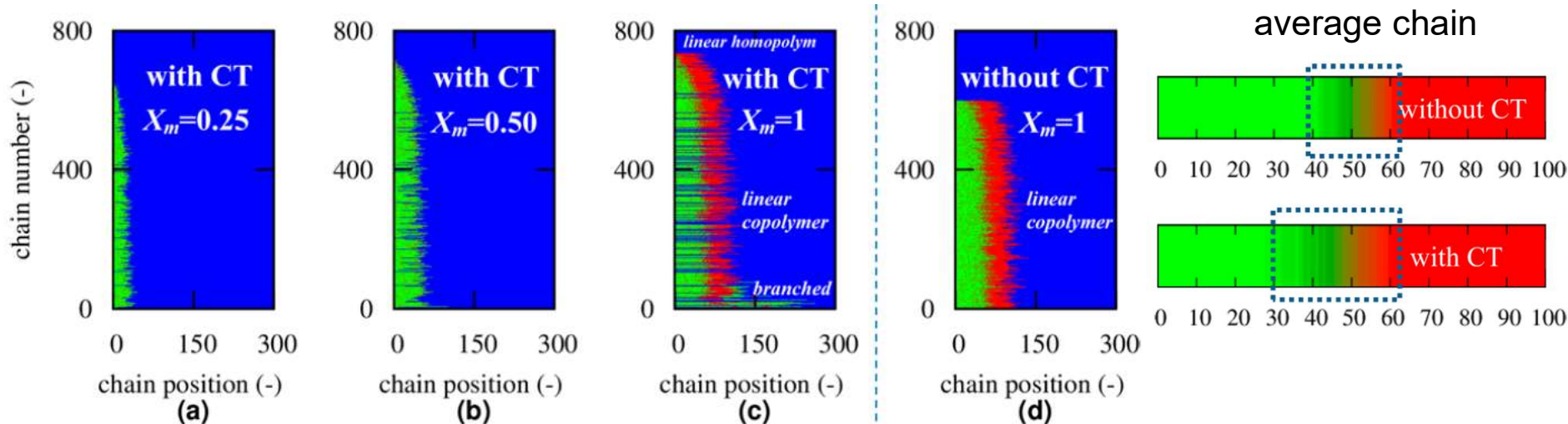
$T = 140\text{ }^{\circ}\text{C}$; $[\text{MeOx}]_0 : [\text{PhOx}]_0 : [\text{MeOTs}]_0 = 50:50:1$; $[\text{MeOx}]_0 + [\text{PhOx}]_0 = 3\text{ mol L}^{-1}$; acetonitrile

1 (MeOx), 2 (PhOx)

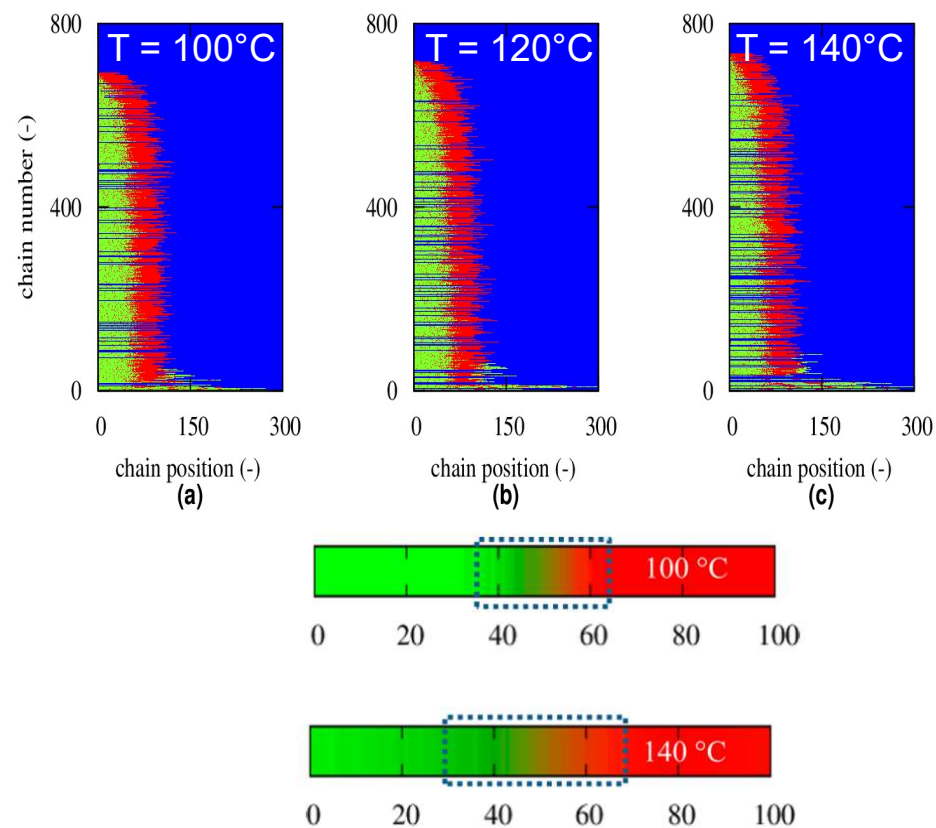
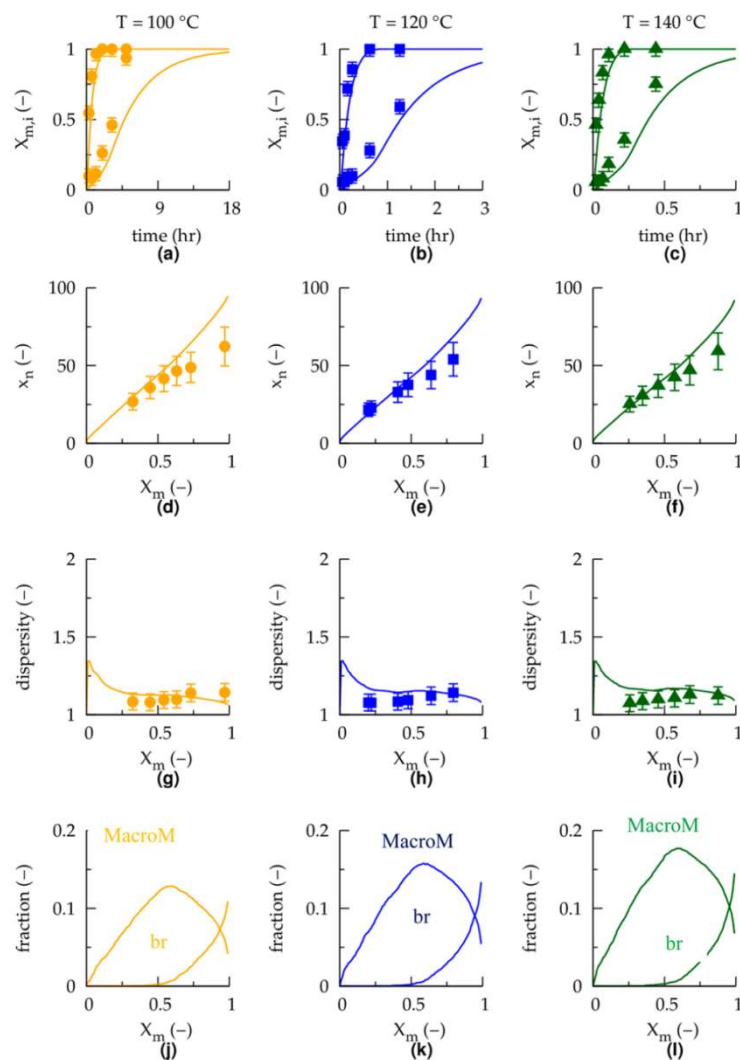


Effect of chain transfer in CROcoP (2)

T= 140 °C; [MeOx]₀: [PhOx]₀: [MeOTs]₀ = 50:50:1; [MeOx]₀ + [PhOx]₀ = 3 mol L⁻¹; solvent: acetonitrile



Effect of temperature



Conclusions

- Matrix-based kinetic Monte Carlo modeling enables visualization of the complete microstructure for each individual macromolecule and is a powerful tool to understand and improve controlled polymerization processes
- Complemented with ab initio calculations and combined with experimental studies the developed modeling tools allow a detailed exploration of a given polymer chemistry

Acknowledgements

- national collaborations

- Prof. F. Du Prez
- Prof. R. Hoogenboom
- Prof. Ph. Dubois
- Prof. T. Junkers



- International collaborations

- Prof. K. Matyjaszewski
- Prof. C. Barner-Kowollik
- Prof. M. Coote
- Prof. R.A. Hutchinson
- Prof. M.F. Cunningham
- Prof. M.J. Monteiro
- Dr. J.F. Lutz

Thank you for your attention!!!

